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# Thermogravimetric study of GaAs chlorination between -30 and $900 \,^\circ C$

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# ABSTRACT

Gallium (as GaAs) is at present an essential part of electronic devices, and the recovery of this element from electronic wastes is fundamental for the metallurgic industry. In this work, with the aim of recovering Ga by chlorination, the following reaction was investigated:

 $GaAs(s) + 3Cl_2(g) \rightarrow GaCl_3(s, g, l) + AsCl_3(s, g, l)$ 

A thermogravimetric study of the previous reaction was carried out, and the following variables were investigated: chlorine partial pressure, in the range between 0.2 and 1 atm, by dilution with  $N_2$  and reaction temperature in the -29 °C to 900 °C interval. The thermodynamic calculations predicted that the reaction was feasible during the entire analyzed temperature range, and the experimental results were in agreement with the thermodynamic estimations. The results showed that the chlorination rate did not change significantly with temperature, but it increased with the chlorine partial pressure. It was found that AsCl<sub>3</sub> was partially evaporated at temperatures above 20 °C, while the GaCl<sub>3</sub> started evaporating at 100 °C. The experimental observations showed that the mechanism originating the reaction was different in each temperature range ranging between -30 and 160 °C, 200-400 °C, and above 500 °C. In the first case the reaction was caused by adsorption of Cl<sub>2</sub> on the solid surface. In the second case, the solid started reacting when little quantities of GaCl<sub>3</sub> and AsCl<sub>3</sub> vapor were injected in the entrance of the system, indicating that the chlorination kinetics responded to an autocatalytic mechanism. Above 500 °C, the reaction was caused without adding chlorination products. The results of the analysis by scanning electron microscopy and X-ray diffraction showed a preferential attack on one of the crystal planes of GaAs. Besides, the formation of  $Ga_2O_3$  and  $GaAsO_4$  was observed as a consequence of the presence of small quantities of oxygen accompanying Cl<sub>2</sub>.

The results showed that chlorination is a selective and economic methodology for the recovery of gallium from electronic wastes.

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### 1. Introduction

Gallium is a rare element with a natural abundance of 16 ppm. Although this mineral is more concentrated in gallite, it is mostly found in aluminosilicates such as bauxite, clays and zinc ores for example, sphalerite). Gallium is mainly extracted from wastes obtained during aluminium processing, and also from electrolytic zinc condensers. Other extraction sources include ashes released from coal burning [1].

Gallium metal, alloys and compounds are used in a relatively reduced scale in industries such as the construction of machines, the production of electrical and electronic equipment (diodes, tran-

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sistors, lasers, conductors coating), vacuum technology, and in the chemical industry for the catalyzers manufacturing [1].

Gallium has important applications in optoelectronics (LED's), telecommunications, aerospace technology, and many commercial and domestic devices such as computers and DVD's [1].

Gallium has found application in the Gallex Detector Experiment located in the Gran Sasso Underground Laboratory in Italy. In this experiment, 30.3 tons of gallium in the form of 110 tons of GaCl<sub>3</sub>–HCl solution are being used to detect solar neutrinos [2].

When gallium is used for glass painting, it forms a brilliant mirror and also wets the crystal and porcelain. The element adapts easily to form alloys of low fusion point (for example, eutectic alloys) with most metals.

Gallium arsenide (GaAs) is a valuable compound widely used in the manufacturing of advanced semiconductors for microwave transceivers, transistors, solar cells, lasers, laser diodes, compact discs and other electronic applications. This compound has several advantages in relation to other semiconductor materials, such as

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Fig. 1. Change of Gibbs free energy versus temperature for the GaAs chlorination reaction.

fast operation with low energy consumption, good radiation resistance and capacity to convert electrical signals into optical ones [1,3].

The manufacturing of electrical and electronic devices has rapidly developed, giving place to an increase in the production of wastes from these devices. The recycling of these wastes is an important issue not only because their reduction is necessary but also because valuable materials can be recovered. Besides, these kinds of wastes constitute a concern for the governments and also for the population due to their dangerous materials [4].

Electronic wastes are of diverse complexity due to their different materials and components and to the different processes used for the equipment manufacturing. The characterization of these wastes is of key importance for the development of a recycling system with a good cost-benefit relation between the system and the environment. The selective dismantling used to identify dangerous substances and/or valuable materials is an essential process in the recycling of these wastes [5].

Progress in the development of materials with application in different fields, ranging from medicine to aerospace industries, has made the production of high purity metals necessary. Several methods exist to produce rare and precious metals with a high purity degree; however, liquid–liquid extraction from metallic halides in solution and chlorides distillation are the most widely applied methodologies nowadays. In both cases, obtaining the metallic halides is the first stage of the process, and one of the most widely used techniques for this stage is the previous chlorination of materials such as metals, ores, metallic oxides or industrial wastes [6].

The use of chlorination in the metal extraction processes by means of pyrometallurgical and hydrometallurgical methods has received great attention in recent decades, and an increasing use of the chlorine chemistry is expected due to the advantages of this process [7]. According to Kubo et al. [8], the main advantages of the chlorination process in relation to other refinement methods for gallium recovery from GaAs can be summarized as follows: operation temperatures are low, most of the impurities can be effectively eliminated, high-purity metallic gallium can be obtained and the productivity increase is significant.

Several authors have reported the mechanism of the chlorination reaction of GaAs. Jenichen and Engler [9], using the functional density method, theoretically found that the most feasible reaction mechanism involves adsorption of Cl<sub>2</sub> on the surface of GaAs and subsequent desorption of GaCl. Hung et al. [10] studied the chlorination of GaAs at low temperatures (110 K) using soft X-ray photoelectron spectroscopy and found that at low exposures of Cl<sub>2</sub> it dissociates itself and preferentially adsorbs on the atoms of As inducing the breaking of the bond Ga–As, generating subsequently gallium and arsenic chlorides. Bond et al. [11] using pulsed supersonic molecular beam scattering studied the reaction of Cl<sub>2</sub> with the surface of GaAs, and they observed that the reaction products depended on the flow of chlorine and temperature; at low flows of Cl<sub>2</sub> and high temperature, the formation of GaCl and As predominates, and at high flows of Cl<sub>2</sub> and low temperature, there is a predominance of GaCl<sub>3</sub> and AsCl<sub>3</sub> formation.

This paper presents the thermogravimetric study of GaAs chlorination with  $Cl_2$  between -30 and 900 °C. The partial pressure of  $Cl_2$  was varied between 0.2 and 1 atm. The purpose of the study is to provide data to facilitate elucidating the mechanism and kinetics of the reaction in working conditions so that these results can then be applied to the recovery of Ga.

#### 2. Thermodynamic analysis

This section presents the thermodynamic calculations for the GaAs–Cl<sub>2</sub> system, which have been done for the temperature range used for the experimental essays. All the calculations were obtained using the HSC Chemistry for Windows, version 5.1 software [18].

The reactions that may occur between GaAs and  $Cl_2$  have been theoretically and experimentally studied by several authors [9–17] under different temperature conditions, partial pressure and  $Cl_2$ quantity in order to obtain components for electronic applications. The results of these investigations showed that the reaction products vary in their composition as well as in their aggregation state according to the working conditions.

A first analysis involves to study the feasibility of a gallium and arsenic chlorides formation from GaAs. Fig. 1 shows the results of the calculation of the Gibbs free energy variation for the following global reaction:

$$GaAs + 3Cl_2(g) \rightarrow GaCl_3(s, l, g) + AsCl_3(s, l, g)$$
(1)

The analysis of Fig. 1 permits to conclude that the reaction between GaAs and  $Cl_2$  is feasible at all the studied temperature



Fig. 2. Equilibrium composition in pure chlorine.

range, showing greater spontaneity as temperature decreases. The changes in the graph slope indicate phase changes of the reaction products. It is important to emphasize that between 150 and 360 °C the formation of the gaseous gallium trichloride is more feasible as dimmer  $Ga_2Cl_6$ .

The equilibrium compositions at different temperatures and  $Cl_2$  amounts was used to present the thermodynamic analysis for the reaction between GaAs and  $Cl_2$ .

The equilibrium compositions were obtained assuming that from the elements constituting the reagents used, all the species available in the software database may be formed: As(g), As<sub>2</sub>(g), As<sub>3</sub>(g), As<sub>4</sub>(g), AsCl<sub>3</sub>(g), Cl<sub>2</sub>(g), Cl<sub>2</sub>(g), Cl<sub>3</sub>(g), Cl<sub>4</sub>(g), Ga(g), Ga<sub>2</sub>(g), GaAs(g), GaCl(g), GaCl<sub>2</sub>(g), GaCl<sub>3</sub>(g), Ga<sub>2</sub>Cl<sub>2</sub>(g), Ga<sub>2</sub>Cl<sub>4</sub>(g), Ga<sub>2</sub>Cl<sub>6</sub>(g), AsCl<sub>3</sub>(1), Ga(1), As(1), GaCl<sub>3</sub>(1), As(A) (amorphous arsenic), As(Y) (yellow arsenic, cubic), Ga(s), As(s), GaAs(s), GaCl<sub>3</sub>(s).

Fig. 2 shows the equilibrium composition for the GaAs–Cl<sub>2</sub> reacting system in the temperature range ranging between -30 and 1000 °C obtained considering a total pressure of the system of 1 atm. The initial reagents were GaAs(s) and Cl<sub>2</sub>(g). The quantity of Cl<sub>2</sub>(g) was higher than the stoichiometric. Since the experimental assays were carried out with excess Cl<sub>2</sub>, the estimates were performed with excess Cl<sub>2</sub> in relation to the reaction using the largest quantity of Cl<sub>2</sub> (reaction (1)). The composition was in the same figure it can be observed that in all the analyzed temperature range, the reaction products are gallium trichloride and arsenic trichloride which are formed according to reaction (1), with different aggregation states depending on the temperature.

Fig. 3 shows the equilibrium composition in relation to  $Cl_2$  quantity. This diagram was calculated at a total pressure of 1 atm, with pure  $Cl_2$  at 85 °C, starting with one mol of GaAs and increasing the quantity of  $Cl_2$ . It can be observed that as GaAs(s) is consumed and GaCl<sub>3</sub>(1) and As(s) are produced; when all the GaAs has been consumed, the formed As starts reacting with the  $Cl_2$  producing AsCl<sub>3</sub>(1).

While Fig. 2 provides a thermodynamic estimation of the species that may exist in equilibrium at different temperatures when GaAs reacts with  $Cl_2$  in excess, Fig. 3 shows the thermodynamic evolution of the reaction in relation to the amount of the present chlorine, which might be useful to elucidate the most probable reaction mechanism.

Fig. 4 shows the partial pressure variation in relation to temperature for the three products that may be formed by the reaction between GaAs and Cl<sub>2</sub>. AsCl<sub>3</sub> vapor pressure reaches  $10^{-3}$  atm at 58 °C, where as Ga<sub>2</sub>Cl<sub>6</sub> reaches this pressure at 118 °C, and GaCl<sub>3</sub>, at 125 °C.



Fig. 3. Effect of Cl<sub>2</sub> quantity at 85 °C.

The formation of small amounts of oxygenated compounds, such as  $Ga_2O_3$  and  $GaAsO_4$  was observed (see Section 4.2.1) in the experimental phase when working at a temperature above 300 °C. In order to investigate this phenomenon, the analysis of the compounds thermodynamic feasibility to be formed from the chlorination products of the gallium arsenide was carried out.

The results shown in Fig. 5a indicate that the reactions of the compounds formation are thermodynamically feasible at almost all the studied temperature range, except for the reaction of the  $Ga_2O_3$  formation which is spontaneous up to 810 °C. Also, the predominance diagrams ( $pO_2$  versus  $pCl_2$ ) presented in Fig. 5b and c for Ga and As, respectively, show that Ga and As oxygenated compounds predominate over those chlorinated at 25 °C.

# 3. Experimental

#### 3.1. Materials

The materials used were GaAs Sigma–Aldrich with a purity of 99.999%, gaseous chlorine INDUPA Argentina with a purity of 99.5% and  $N_2$ , as gas for dilution and purge, AGA ARGENTINA with a purity of 99.9%.



Fig. 4. Partial pressure of equilibrium versus temperature for  $AsCl_3,\,Ga_2Cl_6$  and GaCl\_3.



Fig. 5. (a) Change of Gibbs free energy in relation to temperature for the reactions which include the formation of oxygenated compounds. (b) Predominance diagrams (pO<sub>2</sub> versus pCl<sub>2</sub>) for Ga. (c) Predominance diagrams (pO<sub>2</sub> versus pCl<sub>2</sub>) for As.



Fig. 6. Isothermal chlorination of GaAs with pure Cl<sub>2</sub>, in the temperature range between -30 and 200 °C.

#### 3.2. Experimental equipment and procedure

The monitoring of the chlorination reaction was performed using thermogravimetry. An experimental equipment capable of working in corrosives and no corrosives atmospheres, developed in our laboratory [19], was used for this purpose.

The analyses of the chlorination wastes were carried out using X-ray diffractometry (XRD) in a Rigaku equipment model D-Max III C; X-ray fluorescence (XRF) using a Philips equipment model PW 1400; scanning electron microscopy (SEM) and electron probe microanalysis (EPMA) using a LEO 1450VP microscope and a coupled EDAX Gemini 2000 energy dispersive spectrometer (EDS) and atomic absorption spectrometry (AAS) using a Shimadzu 6800 AA equipment.

The experimental procedure for the thermogravimetric study of GaAs chlorination was as follows: the sample, previously ground and classified to a particle size of -40+90 mesh, was placed in a previously weighed quartz crucible, then the crucible with the sample was supported in a thermobalance. In each experiment a mass of solid reagent of approximately 50 mg was used.

After being placed in the thermogravimetric system, the sample was thermostatized for 30 min in an  $N_2$  current of 50 ml/min. Once the working conditions were stabilized, the  $N_2$  flow was turned off and a Cl<sub>2</sub> current of 50 ml/min was introduced in the thermogravimetric system at the corresponding partial pressure by dilution with  $N_2$ ; time was measured from this moment, and data of mass change were collected. When the experiment was finished the Cl<sub>2</sub> gas flow was turned off and the thermogravimetric system was purged with  $N_2$ . In all the essays the thermostatization and purge

times were standardized in an  $N_2$  environment. After that, the crucible with the chlorination wastes was removed, and the wastes were prepared for analysis. The effluent gases from the reactor were treated by  $H_2SO_4$  and NaOH traps.

### 4. Results and discussion

Isothermal essays at different temperatures and partial pressures of chlorine were carried out until complete conversion of GaAs in order to study the influence of both variables on the chlorination reaction.

The thermogravimetric analysis of the GaAs–Cl<sub>2</sub> system is presented separately for temperature ranges lower and higher than  $200 \,^{\circ}$ C.

#### 4.1. Thermogravimetric analysis between –30 and 200°C

#### 4.1.1. Temperature effect

The effect of temperature on the reaction between GaAs and pure  $Cl_2(g)$  was analyzed from thermogravimetric measurements. Fig. 6 shows the results of the time evolution of relative mass changes. There is an induction time of approximately 1 min at all the studied temperatures whose origin will be discussed in Section 4.3. The maximum relative mass changes obtained from Fig. 6 are shown in Table 1 close to the expected values for the temperatures at which aggregation states of reaction products can be assumed. For other temperatures the mass change contribution of vaporization process of reaction products) cannot be theoretically predicted

#### Table 1

Mass percentage changes expected in relation to the aggregation state of the products.

Reaction		Maximum theoretical mass change (5%)	Temperature (°C)	Maximum experimental mass change (%)	x
$GaAs + 3Cl_2(g) \rightarrow GaCl_3(s) + AsCl_3(l)$	(1)	148.15	-29	154.59	
$GaAs+3Cl_2(g)\rightarrowGaCl_3(l)+AsCl_3(l)$	(2)	148.15	-10	144.81	
$GaAs + 3Cl_2(g) \rightarrow GaCl_3(l) + (1 - x)AsCl_3(l) + xAsCl_3(g)$			10	139.58	0.06
$GaAs + 3Cl_2(g) \rightarrow GaCl_3(l) + (1 - x)AsCl_3(l) + xAsCl_3(g)$			30	118.23	0.23
$GaAs + 3Cl_2(g) \rightarrow GaCl_3(l) + (1 - x)AsCl_3(l) + xAsCl_3(g)$			50	101.89	0.36
$GaAs + 3Cl_2(g) \rightarrow GaCl_3(l) + (1 - x)AsCl_3(l) + xAsCl_3(g)$			85	78.02	0.55
$GaAs+3Cl_2(g)\rightarrowGaCl_3(l)+AsCl_3(g)$	(3)	21.73	110	21.96	
$GaAs + 3Cl_2(g) \rightarrow (1-x)GaCl_3(l) + xGaCl_3(g) + AsCl_3(g)$			160	-82.32	0.88
$GaAs+3Cl_2(g)\rightarrowGaCl_3(g)+AsCl_3(g)$	(4)	-100	200	-94.55	



Fig. 7. Ga and As loss in the chlorination essays at different temperatures.

but empirically quantified through the calculation of the stoichiometric coefficient *x*, as shown in last column of Table 1. Also, at low temperatures, absorption of  $Cl_2$  (b.p. =  $-34.04 \circ C$ , [2]) in liquid chlorides must be taken into account. Finally, chlorides vaporization could be enhanced by a local temperature rising due to reaction exothermic effect. Therefore, chemical equations (1), (2) accounts well for reaction at  $-29 \circ C$  and  $-10 \circ C$ , respectively, and reaction at  $10 \circ C$  deviates slightly from mass changes predicted by equation (2) indicating a low contribution ( $x \approx 0$ ) of AsCl<sub>3</sub>(1) vaporization. As the temperature rise from  $30 \circ C$ , the increasing *x* values indicates the enhancing contribution of AsCl<sub>3</sub>(1) vaporization. In fact, for experiments carried out at  $50 \circ C$  and  $85 \circ C$  (Fig. 6), once reaction finished, a continuous mass decreasing corresponds to AsCl<sub>3</sub>(1) vaporization as unique phenomenon.

Total mass change after chlorination at  $110 \,^{\circ}$ C is accounted for total vaporization of AsCl<sub>3</sub> (chemical equation (3)) which, despite temperature is lower to its boiling point ( $130 \,^{\circ}$ C [2]), can be explained from the exothermic effect above mentioned. The experiments at highest temperatures are interpreted taking into account GaCl<sub>3</sub>(g) or Ga<sub>2</sub>Cl<sub>6</sub>(g) formation which is partial at 160  $\,^{\circ}$ C and is nearly total at 200  $\,^{\circ}$ C.

Also reaction residues where quantified by atomic absorption measurements and results are shown in Fig. 7 as Ga and As relative mass loss. Fig. 7 quantitatively agree with the increasing AsCl<sub>3</sub>(1) vaporization at temperatures greater than 10 °C, and partial GaCl<sub>3</sub>(1) vaporization for the highest temperatures, as determined from thermogravimetric measurements.

## 4.1.2. Effect of the partial pressure of Cl<sub>2</sub>

Figs. 8-10 the results of the thermogravimetric essays carried out to investigate the effect of the Chlorine partial pressure, pCl<sub>2</sub>, (using N<sub>2</sub> as inner diluent gas) at -20, 20 and 85 °C, respectively. For all tested temperatures, the greater pCl<sub>2</sub>, the greater the reaction rate (with the only exception shown in Fig. 10 for the two highest pCl<sub>2</sub>). However, a detailed analysis is not easy because chlorination reaction is overlapped with chlorides evaporation. Therefore, any reaction order calculation, for example, will be falsified by other processes. Moreover, observed maximum relative mass changes indicates that contribution of chlorides vaporization seems to be dependent, not only on temperature (x value in Table 1) but also on pCl<sub>2</sub>. The net effect for lower pCl<sub>2</sub> is some combination of  $N_2$ dilution, that enhances the heat dissipation and reduces the mentioned exothermic effect on chlorides vaporization, and a lowering in chlorination rate enhances the relative contribution of chlorides vaporization. This complexity is also confirmed by the (unexpected)



**Fig. 8.** Influence of  $Cl_2$  partial pressure of at -20 °C.



Fig. 9. Influence of Cl<sub>2</sub> partial pressure at 20 °C.

inverse dependence of reaction rate process with  $pCl_2$  observed at 85 °C as above mentioned from Fig. 10.

#### 4.2. Thermogravimetric analysis between 300 and 900 °C

#### 4.2.1. Temperature effect

Chlorination performed at this temperature range exhibits a particular behavior. For the tested temperatures below 600 °C reaction does not start unless small amounts of a GaCl<sub>3</sub>(g)–AsCl<sub>3</sub>(g) mixture is added. Therefore, for the experiments at 300 °C and 500 °C, those chlorides were injected in Cl<sub>2</sub> flow and supply was finished once reaction was started.

Fig. 11 shows the results of the thermogravimetric study of the GaAs chlorination with pure chlorine at temperatures between 300 and 900 °C. According to the thermodynamic predictions analyzed in Section 2, all the products of the GaAs chlorination are in gaseous state in this temperature range, and in a flow system, they may be carried away by the gaseous current and then condensed outside the reaction zone. Consequently, the expected relative mass loss might be 100%.

Fig. 11 shows that chlorination rate does not practically depend on temperature; induction time changes inversely with temperature and, excepting for the two highest temperatures, solid residues remain (see Section 4.2.3). After chlorinations, solid residues of white color were observed deposited, not also in crucible, but also in reactor walls.

Fig. 11 also shows that solid residues remain, except in the essays performed between 800 and 900 °C. It was observed in the experimental study that the residues were deposited in the crucible and also in the reactor walls. The residues observed in this figure, according to the analyses carried out using SEM, EPMA and XRD, correspond to compounds containing Ga, O and As. These data indicate that the GaAs chlorination was complete, and consequently the masses found at the end of the reaction were due only to these oxygenated compounds. The formation of these residues, whose origin, composition and structure will be discussed in detail in Section 4.2.3, might be due to the reactions between the products of the GaAs reaction and small amounts of  $O_2$  present in the Cl<sub>2</sub> (Fig. 5).

#### 4.2.2. Effect of the Cl<sub>2</sub> partial pressure

Figs. 12 and 13 show the effect of  $pCl_2$  on reaction rate at 300 °C and 500 °C, respectively. The effect of  $pCl_2$  on reaction rate is less prominent as  $pCl_2$  decreases. In all cases, final relative mass change indicates variable amounts of solid residues. At both temperatures,



Fig. 10. Influence of Cl<sub>2</sub> partial pressure at 85 °C.



Fig. 11. GaAs isothermal chlorination with pure Cl<sub>2</sub>, between 300 and 900 °C.



Fig. 12. Influence of Cl<sub>2</sub> partial pressure at 300 °C.

these solid residues were black or white, respectively, at lower or higher  $pCl_2$  (see Section 4.2.3).

# 4.2.3. Characterization of the solid residues

Solid residues of chlorinations performed at temperatures between 300  $^\circ C$  and 900  $^\circ C$  were analyzed by XRD, SEM and EPMA.

Fig. 14 shows the X-ray diffractograms of residues after reaction with pure Cl<sub>2</sub> at 300 °C, 350 °C and 400 °C and it can be clearly observed that solids in all cases are amorphous. The SEM images and EPMA analyses on these solids were all similar. Fig. 15 shows results corresponding to residue obtained at 350 °C. Solid particles exhibits irregular surfaces and are composed by As, Ga and O. This last result is consistent with the above mentioned white color of



Fig. 13. Influence of Cl<sub>2</sub> partial pressure at 500 °C.



Fig. 14. Diffractograms of the residues from the essays with pure Cl<sub>2</sub>. (a) 300 °C; (b) 350 °C; (c) 400 °C.

residues observed at high  $pCl_2$  if it is assumed residues formed by As/Ga oxides.

Fig. 16 shows the X-ray diffractograms of residues after reaction with pure Cl<sub>2</sub> at 500 °C and 700 °C. residues are clearly crystalline solids. Solid obtained at 500 °C is a mixture of Ga<sub>2</sub>O<sub>3</sub> [21,22] and GaAsO<sub>4</sub> [23]. At 700 °C an additional, and unknown, crystalline phase also appears.

The formation of oxygenated species during chlorinations is explained from  $O_2$  traces presence in commercial  $Cl_2$ , originated at its industrial production. The appearance of these oxides, inside and outside the crucible, likely indicates they are originated by the oxidation of the GaCl<sub>3</sub>(g) and AsCl<sub>3</sub>(g) which are feasible reactions according to Fig. 5. This assumption is also supported by the fact GaAs does not react with air below 800 °C (results not shown).

Fig. 17 shows X-ray diffractograms of residues obtained after chlorinations for  $pCl_2 = 0.2$  atm at 300 °C and 500 °C. XRD peaks allow to identify both solids as GaAs [24], which explain the above mentioned black color of residues observed at low  $pCl_2$ . The diffractogram of the residue obtained at 500 °C shows a high preferred orientation effect of planes (220). Likely  $Cl_2$  through a selective attack promotes changes in crystallites enhancing morphological importance of those planes. Fig. 18 shows the SEM observations of residue obtained at 300 °C compared with starting GaAs confirm a localized reactivity on solid particles.

The absence of oxygenated compounds is consistent with the low  $O_2$  content for pCl<sub>2</sub> = 0.2 atm.

Finally, the residues composition dependence on pCl<sub>2</sub> (some combination of GaAs and As–Ga–O compounds) explain the variable limit for mass loss for experiments carried out with low pCl<sub>2</sub> (Figs. 12 and 13) and the incomplete products vaporization for experiments with pure Cl<sub>2</sub> (Fig. 11) due to formation of non reactive As–Ga–O compounds after complete GaAs chlorination.

#### 4.3. Reaction mechanism

GaAs chlorination shows two main behaviors depending on temperature. As mentioned, chlorination were performed in a simple experimental procedure at all temperatures, except for the range between 300 °C and 500 °C. For this temperatures the reaction does not start when  $Cl_2$  reaches GaAs, unless small amounts of a mixture of reaction products (GaCl<sub>3</sub>(g)–AsCl<sub>3</sub>(g)) are added. This last feature corresponds to an autocatalytic behavior.

Any mechanism proposal must explain autocatalytic and non autocatalytic behaviors at each temperature range, and the observed induction time variation with experimental conditions. Each temperature range will be separately discussed.

# 4.3.1. Low temperature range ( $-30\,^\circ\text{C}$ and $200\,^\circ\text{C}$ ). Non catalytic behavior

A first step proposal in chlorination process could be supported on experimental [11,14] and theoretical [15] studies which conclude the GaAs(s)–Cl<sub>2</sub>(g) interaction, at room temperature, yields the formation of GaCl(g) and As<sub>2</sub>(g) or As<sub>4</sub>(g). Therefore, Ga is firstly





Fig. 15. SEM micrographs of the residue from the essay carried out at 350 °C with pure Cl<sub>2</sub>. (a) Residue particle; (b) enlarged surface of the particle; (c) residue analysis of the essay carried out at 350 °C with pure Cl<sub>2</sub>.



Fig. 16. Diffractograms of the residues from the essays carried out with pure  $Cl_2$ . (a) 500 °C; (b) 700 °C.



Fig. 17. Diffractograms of the residues from the essays with a Cl<sub>2</sub> partial pressure of 0.2 atm. (a) 300 °C; (b) 500 °C.

(a)

chlorinated instead As is. Then initiation includes adsorption of Cl<sub>2</sub> on As atoms of GaAs. Adding possible propagation steps, a mechanism could be expressed as:

Stage 1 (initiation)

Ga Ga 
$$\longrightarrow$$
 Ga Ga  $\longrightarrow$  2 GaCl(g) + As<sub>2</sub> or <sup>1</sup>/<sub>2</sub>As<sub>4</sub>(g)  
As As As As As

Stage 2 (propagation)

$$GaCl(g) + Cl_2(g) \rightarrow GaCl_2(g) + Cl(g) or GaCl_3(l,g) \tag{b}$$

$$2GaAs + 2Cl(g) \rightarrow GaCl(g) + As_2 \text{ or } (1/2)As_4(g)$$
(c)

$$GaCl_2(g) + Cl_2(g) \rightarrow GaCl_3(l,g) + Cl(g)$$
 (d)

$$As_2 o(1/2)As_4(g) + 2Cl(g) \rightarrow 2AsCl(g)$$
(e)

$$AsCl(g) + Cl_2(g) \rightarrow AsCl_2(g) + Cl(g) \text{ or } AsCl_3(l,g)$$
(f)

$$AsCl_2(g) + Cl_2(g) \rightarrow AsCl_3(l, g) + Cl(g)$$
 (g)

Assuming control by stage 1, the decrease of induction time as temperature increases (Fig. 6) can be explained based on an increasing rate on GaCl(g) formation, due to the break of Ga–As is favored, which faster increase Cl radicals concentration through the first propagation step, b.

Finally, reaction is sustained due to formation of the very active Cl(g) radicals at several of propagation steps, two of them (d, g) also accounts for GaCl<sub>3</sub> and AsCl<sub>3</sub> products formation.

# 4.3.2. Medium temperature range (300 $^\circ C$ and 500 $^\circ C$ ). Catalytic behavior

As temperature increases  $Cl_2$  adsorption on GaAs could be enoughly unfavorable to avoid the effective participation of step a. The addition of reaction products must generate the reaction initiation. Singh and Krout [20] found that  $AsCl_3$  reacts with GaAs forming GaCl(g), GaCl<sub>2</sub>(g) and As(g) at this temperature range, therefore the following steps, can be added:

$$GaAs + AsCl_3(g) \rightleftharpoons AsCl_2(ads) + Cl(ads) + GaAs$$
 (h)

$$\begin{aligned} &AsCl_2(ads) + Cl(ads) + GaAs \rightarrow AsCl_2(g) \\ &+ GaCl(g) + As_2(ads) + GaAs \end{aligned} \tag{i}$$

$$As_2(ads) \rightarrow As_2(g) \text{ or } (1/2) As_4(g) \tag{j}$$

where Cl radicals are directly formed the initiation step, h. This accounts for decreasing induction time with increasing temperature (Fig. 11) at 300–500 °C range due to acceleration of Cl radicals concentration. Besides, the increase of induction time with decrease of pCl<sub>2</sub> (Figs. 12 and 13) suggests the simultaneous participation of step d whose rate will proportional to Cl<sub>2</sub>(g) concentration. Therefore, once reaction starts catalyzed by gaseous products supply, also propagation steps associated the non autocatalytic regime also operate.

# 4.3.3. High temperature range (600 $^\circ C$ and 900 $^\circ C$ ). Non catalytic behavior

For this temperature range again direct contact between GaAs with  $Cl_2(g)$  is enough to produce chlorination without needing to add reaction products. However for this temperature range step a cannot be considered as for autocatalytic regime. For highest temperature dissociation of  $Cl_2(g)$  can occur. Fig. 19 shows a calculation of amounts of equilibrium species in a  $Cl_2(g)-N_2(g)$  mixture at several temperatures. This diagram shows that the concentration of atomic chlorine Cl(g) is almost null at low temperatures, and as the temperature increases, its molar fraction also increases, and above 500 °C, it is higher than  $10^{-5}$ . This concentration one. The



Fig. 18. SEM micrographs of GaAs particles partially attacked at 300 °C and a Cl<sub>2</sub> partial pressure of 0.2 atm. (a) Original particle of GaAs; (b) residue particles; (c) enlarged zone of one of the particles; (d) surface of an attacked particle.



Fig. 19. Equilibrium diagram of the chlorine species at different temperatures and a  $\mbox{Cl}_2$  pressure of 0.9 atm.

decreasing on induction time observed for increasing temperature for highest range (Fig. 11) can be explained from Fig. 19 because of concentration of Cl radicals increases with temperature.

# 5. Summary

GaAs chlorination with Cl<sub>2</sub> is feasible under several conditions, forming different products according to the environment to which

the system was exposed. The variation of Gibbs standard free energy versus temperature between -30 and 1000 °C shows, for all the proposed reactions that they are thermodynamically feasible in the established direction.

GaAs chlorination with  $Cl_2$  is quite favorable in the temperature range between -30 and 900 °C, and it occurs at a high reaction rate, even at low temperatures. The system, at the studied temperature range, presents three intervals according to the way the reaction starts. Between -30 and 200 °C, the reaction starts by chlorine adsorption on the GaAs surface and the subsequent breakdown of the bond between Ga and As. Between 300 and 500 °C, the behavior is autocatalytic, requiring the presence of a reaction product such as AsCl<sub>3</sub> for the reaction to begin. Above 500 °C, there is a direct reaction between  $Cl_2$  and GaAs due to the formation of atomic chlorine. The reaction temperature has little effect on the chlorination rate although it influences notably the induction times and determines if the reactions products volatilize or remain as solid or liquid residues into the crucible.

In the temperature range between -30 and 200 °C, the reaction is completed in approximately 8 or 9 min. Between -30 and 110 °C, the reaction causes a mass gain, whose magnitude varies according to the working temperature. These mass gains are due to different factors: adsorption of Cl<sub>2</sub> on the sample at -30 °C; at a higher temperature solid and/or liquid products are formed, and a partial evaporation of some species occurs, which is produced by the exothermic effect of the GaAs chlorination reaction. The Cl<sub>2</sub> partial pressure for the different studied temperatures has a marked influence on the chlorination rate, varying the required time to complete the reaction between about 8 min at higher partial pressures and 25 min for the lowest. Also, as in the isothermic essays at constant pressure, the influence of the exothermic effect produced by the chlorination reaction is observed, which causes a partial evaporation of some reaction products, producing a difference between the mass changes expected and those observed.

The chlorination rate of GaAs with pure  $Cl_2$  (1 atm) in the temperature range between 300 and 900 °C is slightly affected by the reaction temperature. Between 300 and 700 °C, and after the reaction is finished, solid residues constituted by  $Ga_2O_3$  and  $GaOAs_4$  remain. The formation of these compounds is due to the interaction in gaseous phase of the trichloride of Ga and As from the chlorination of GaAs and the  $O_2$  contained in the used  $Cl_2$ .

The effect of the partial pressure of  $Cl_2$  on the chlorination rate at 300 and 500 °C is noticeable. The chlorination at 300 °C is completed in approximately 8 and 42 min, working with 1 and 0.2 atm of  $Cl_2$ , respectively. The residues of the chlorination at 0.2 atm contain only GaAs because the reaction stops due to a lack of products in the vapor phase which may continue catalyzing the chlorination reaction.

The reaction mechanism depends on temperature range. At all temperatures steps b–j operates. At temperatures between  $-30 \,^{\circ}$ C and 200 °C, step a must be added as the initiation one. At temperatures between 300 °C and 500 °C, the initiation step involves the step h. Finally, at temperature between 600 °C and 900 °C, the initiation step is Cl<sub>2</sub>(g) thermal dissociation.

#### 6. Conclusions

The results obtained permit to state that GaAs chlorination is a viable methodology to recover Ga and As from GaAs. At low temperature, Ga and As chlorides are in solid and/or liquid state, and the pressure vapor diagrams versus temperature indicate that separation by distillation is feasible.

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